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removing the fine dust inside [the] a reactor [is removed] via filter cartridges[, in particular sintered metal filter cartridges.]; and

passing [the] reaction gas mixture [is passed] to [the] a quench from a dome of the reactor [dome].

2. (Amended) The process as claimed in claim 1, further comprising the step of [wherein] removing a part-stream in the form of a bypass stream having a predetermined fine dust fraction below a predetermined particle size [is removed] from the reactor in addition to the main stream.

3. (Amended) The process as claimed in claim 1 [or 2], wherein the main stream and the bypass stream are removed from separate dome spaces of the reactor.

4. (Amended) The process as claimed in claim 1, further comprising the steps of: [or in any of the following claims, wherein the bypass stream is switched on and off according to an analysis of]

analyzing a catalyst sample and/or a change in the heat transfer and/or a deterioration of the fluidization behavior[.]; and

switching on or off the bypass stream according to said analysis.

5. (Amended) A fluidized-bed reactor[, in particular for the oxychlorination of ethylene, with the use of] using catalyst granules subjected to abrasion, said reactor comprising: [wherein]

at least one baseplate [(4)] having [sintered metal] filter cartridges [(5) is provided] in a [the] dome [(6)] of the reactor (1), wherein the filter cartridges are dipppable [optionally dipping] into [the] an upper region of the fluidized bed [(2)].

01/14 6. (Amended) The fluidized-bed reactor as claimed in claim 5, wherein the dome space [(6)] is divided, above the plate carrying the filter cartridges [(5)] on its lower surface, into at least two chambers [(6, 6a)], each having an outlet [(11)] for a main stream to the quench and a bypass stream [(8)].

7. (Amended) The fluidized-bed reactor as claimed in claim 6, wherein the filter elements [(5a)] coordinated with the bypass [(8)] have pore size differing from that of the fine dust filter cartridges [(5)] for the controlled passage of fine dust fractions.

8. (Amended) The fluidized-bed reactor as claimed in claim 5 [or in any of the following claims], wherein the ratio of filter elements [(5a)] allowing through fine dust to filter cartridges [(5)] retaining the fine dust is [in the region of] approximately 1:9.

9. (Amended) The fluidized-bed reactor as claimed in claim 5 [or in any of the following claims] [wherein the baseplate (4) is provided with] further comprising a cleaning means using [by means of] compressed gas pulses on the baseplate.

10. (New) The process of claim 1, wherein said process is used primarily for the oxychlorination of ethylene.

11. (New) The process of claim 10, wherein said cartridges are sintered metal filter cartridges.

12. (New) The fluidized-bed reactor of claim 5, wherein said filter cartridges are sintered metal filter cartridges.- -